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(54) HIGH OCTANE UNLEADED AVIATION GASOLINE

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- (51) Int. Cl. *C10L 1/182 C10L 1/223*

(2006.01) (2006.01)

(52) U.S. CI. CPC *C10L 1/223* (2013.01); *C10L 1/1824* (2013.01)

(58) Field of Classification Search

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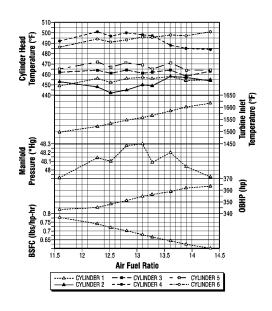
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Primary Examiner — Ellen McAvoy

(57) ABSTRACT

High octane unleaded aviation fuel composition having high aromatics content and CHN content of at least 97.8 wt %, less than 2.2 wt % of oxygen content, a T10 of at most 75° C., T40 of at least 75° C., a T50 of at most 105° C., a T90 of at most 135° C., a final boiling point of less than 190° C., an adjusted heat of combustion of at least 43.5 MJ/kg, a vapor pressure in the range of 38 to 49 kPa is provided.

16 Claims, 16 Drawing Sheets



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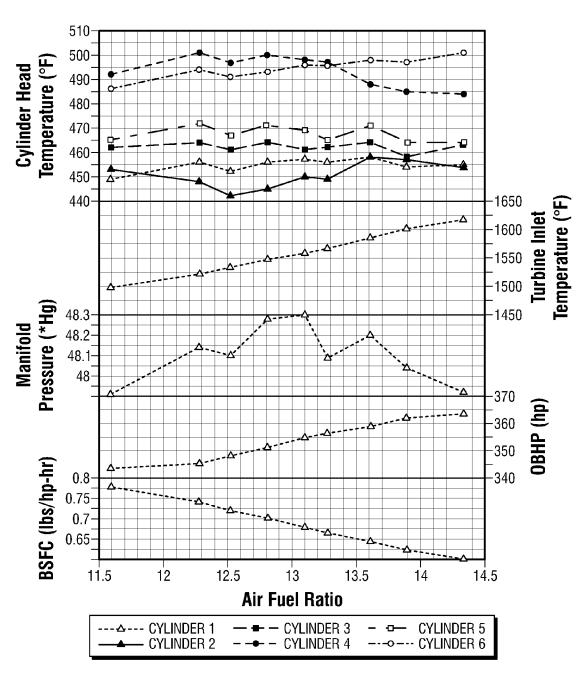


FIG. 1

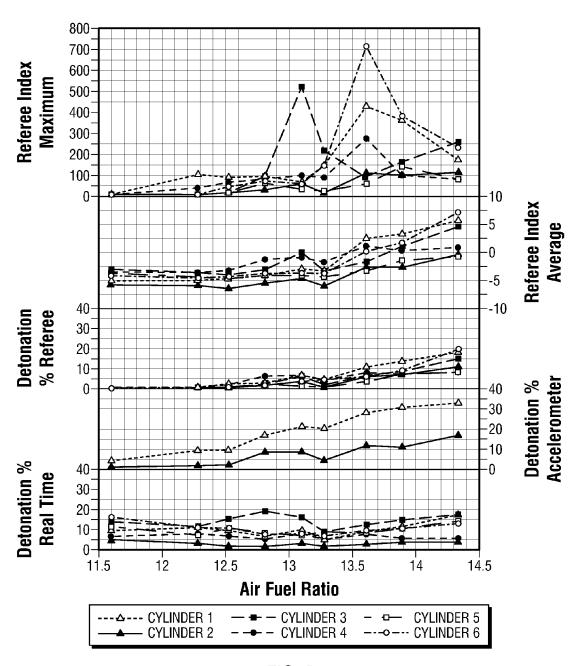


FIG. 2

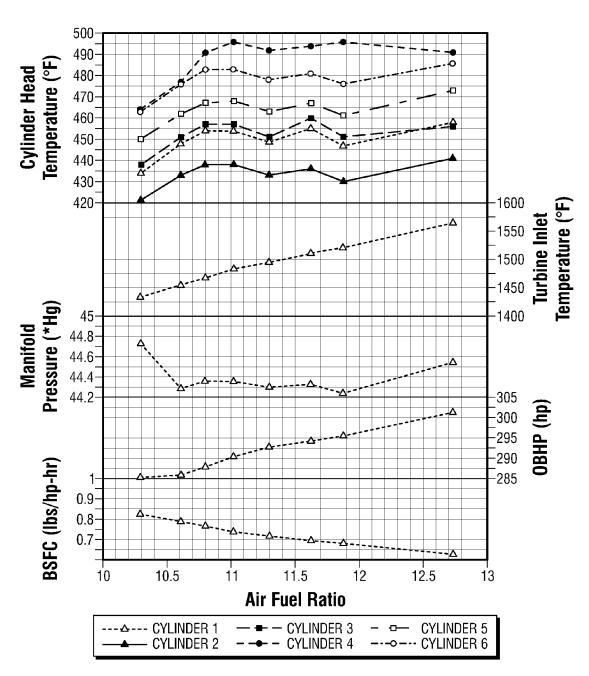


FIG. 3

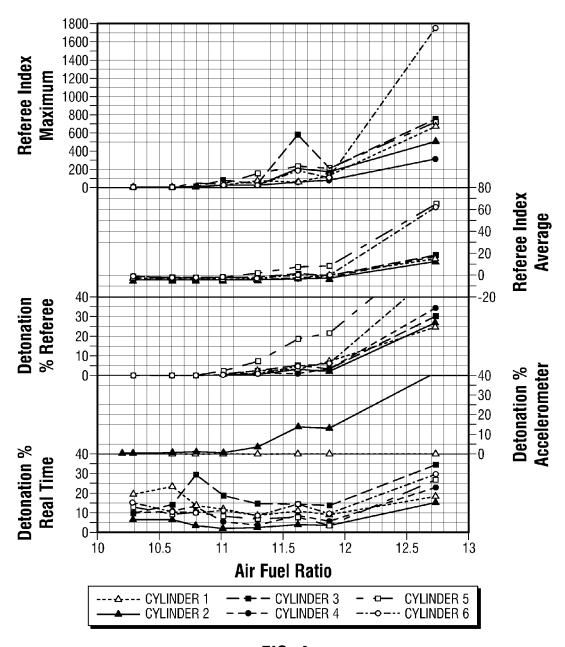


FIG. 4

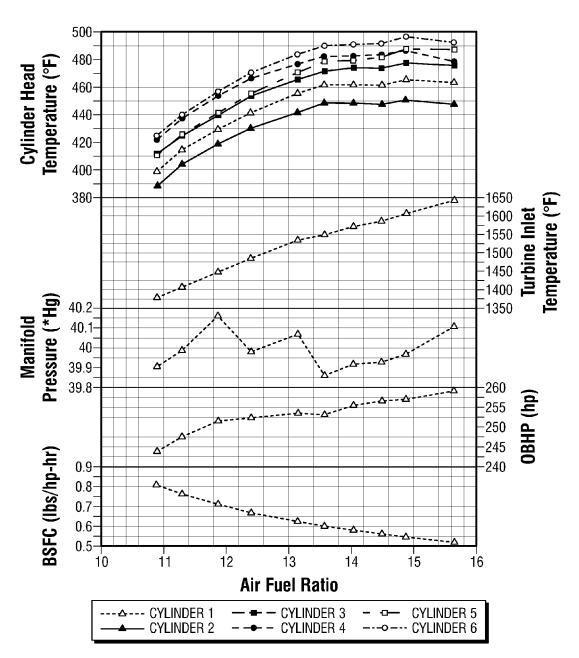


FIG. 5

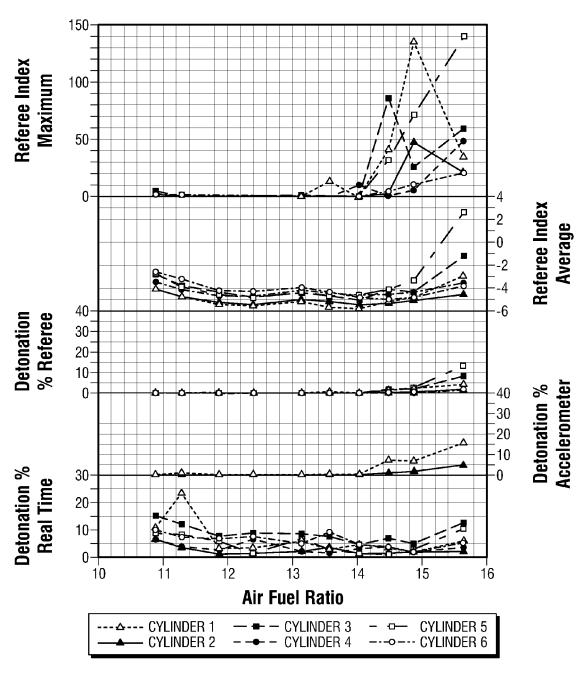


FIG. 6

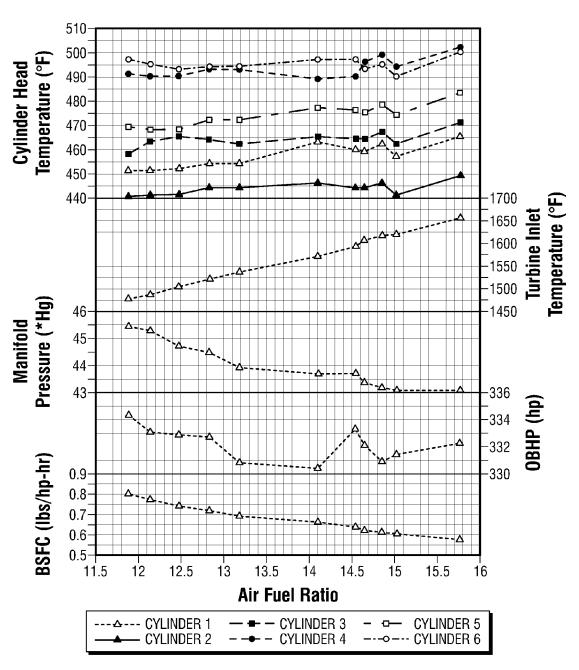


FIG. 7

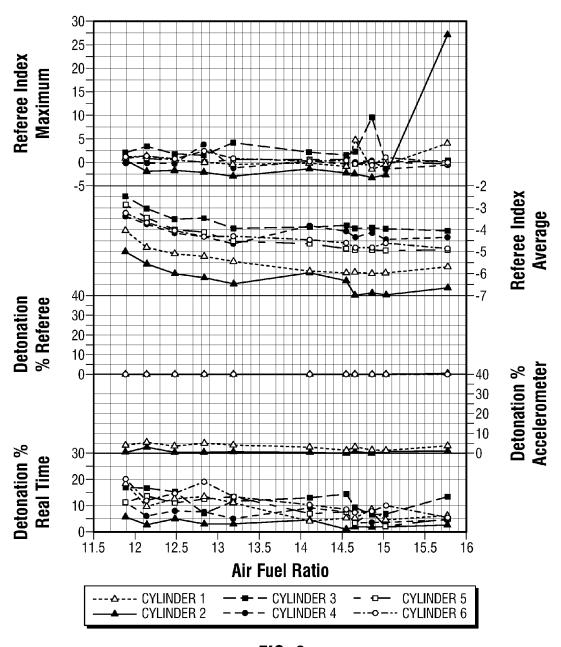


FIG. 8

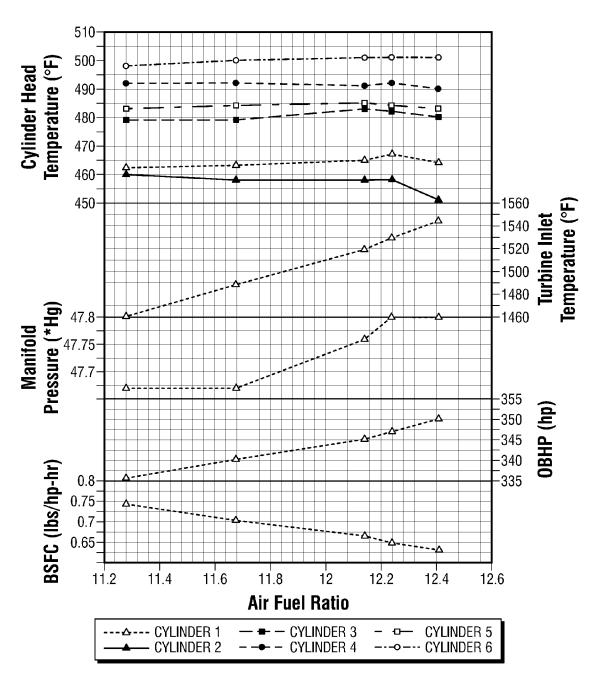


FIG. 9

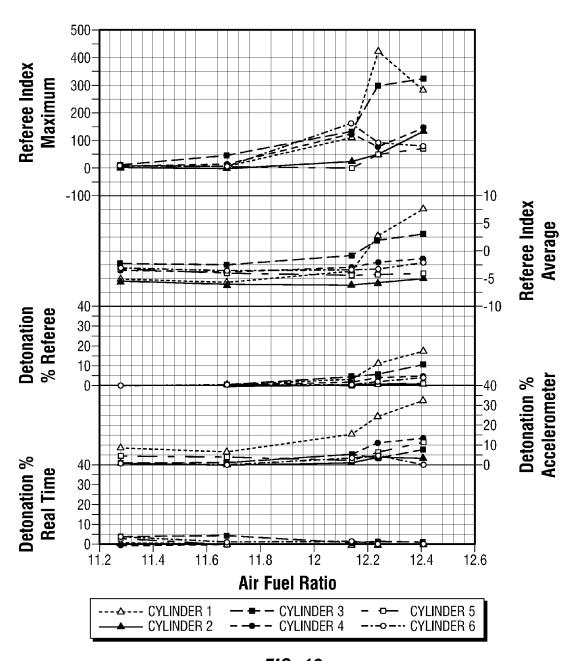


FIG. 10

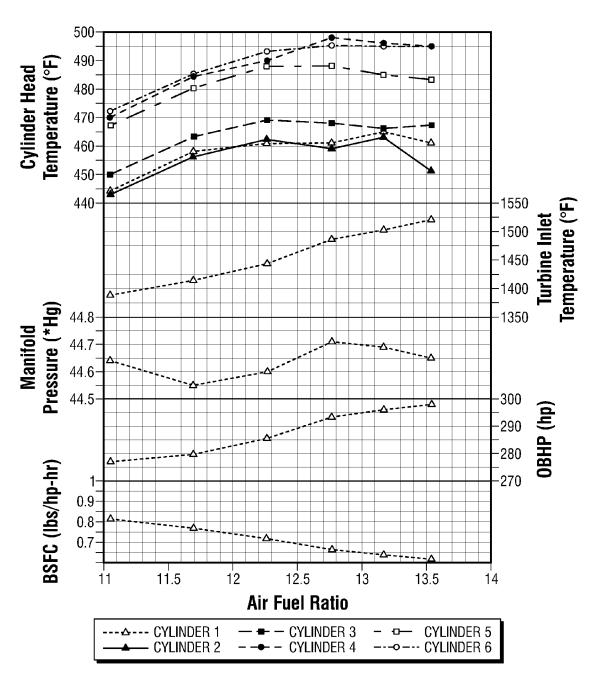


FIG. 11

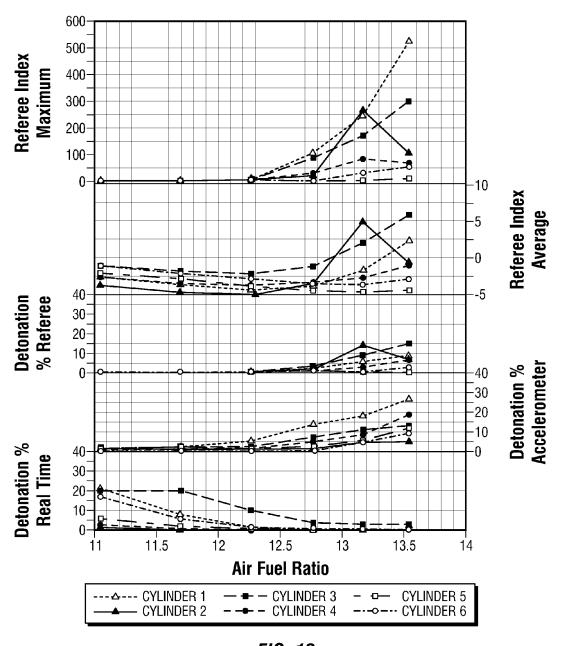


FIG. 12

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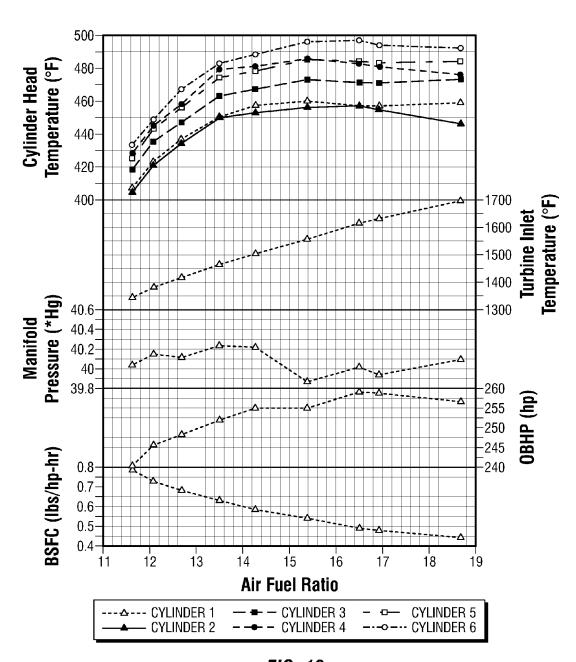


FIG. 13

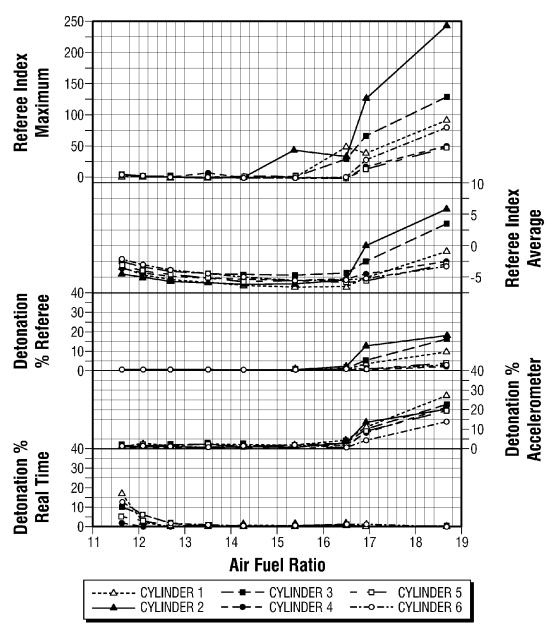


FIG. 14

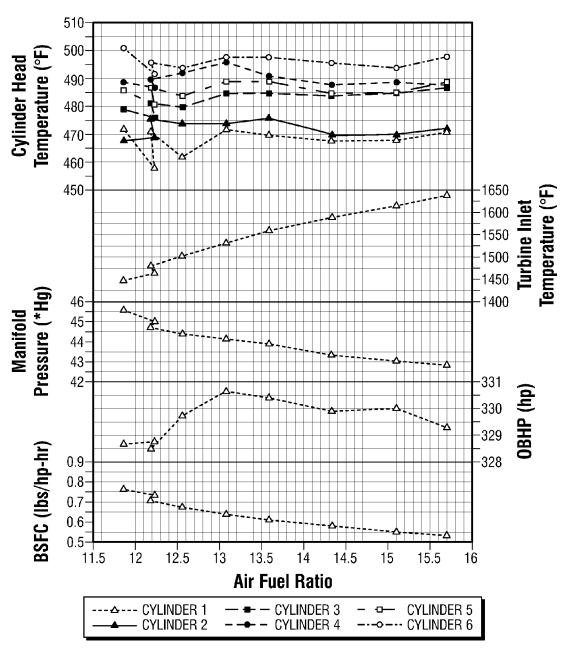


FIG. 15

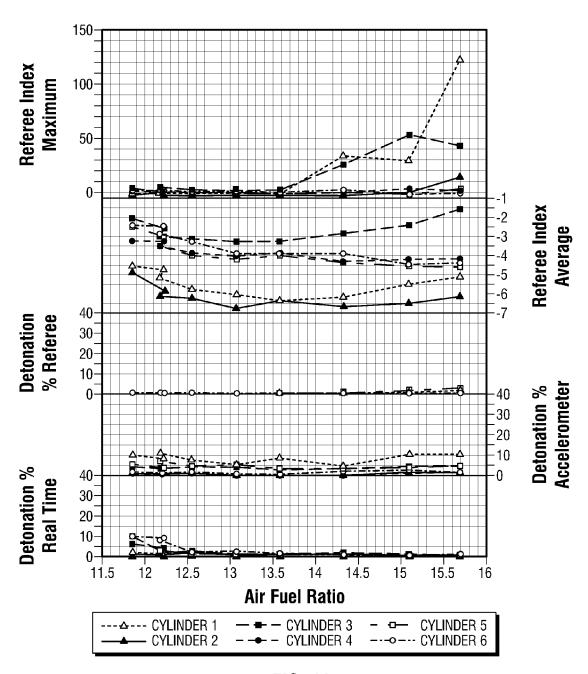


FIG. 16

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HIGH OCTANE UNLEADED AVIATION GASOLINE

This present application claims the benefit of U.S. Patent Application Nos. 61/898,277 filed Oct. 31, 2013, and 61/991, 5940 filed May 12, 2014, the entire disclosures of which are incorporated herein by reference.

FIELD OF THE INVENTION

The present invention relates to high octane unleaded aviation gasoline fuel, more particularly to a high octane unleaded aviation gasoline having high aromatics content.

BACKGROUND OF THE INVENTION

Avgas (aviation gasoline), is an aviation fuel used in sparkignited internal-combustion engines to propel aircraft. Avgas is distinguished from mogas (motor gasoline), which is the everyday gasoline used in cars and some non-commercial light aircraft. Unlike mogas, which has been formulated since the 1970s to allow the use of 3-way catalytic converters for pollution reduction, avgas contains tetraethyl lead (TEL), a non-biodegradable toxic substance used to prevent engine knocking (detonation).

Aviation gasoline fuels currently contain the additive tetraethyl lead (TEL), in amounts up to 0.53 mL/L or 0.56 g/L which is the limit allowed by the most widely used aviation gasoline specification 100 Low Lead (100LL). The lead is required to meet the high octane demands of aviation piston 30 engines: the 100LL specification ASTM D910 demands a minimum motor octane number (MON) of 99.6, in contrast to the EN 228 specification for European motor gasoline which stipulates a minimum MON of 85 or United States motor gasoline which require unleaded fuel minimum octane rating 35 (R+M)/2 of 87.

Aviation fuel is a product which has been developed with care and subjected to strict regulations for aeronautical application. Thus aviation fuels must satisfy precise physicochemical characteristics, defined by international specifica- 40 tions such as ASTM D910 specified by Federal Aviation Administration (FAA). Automotive gasoline is not a fully viable replacement for avgas in many aircraft, because many high-performance and/or turbocharged airplane engines require 100 octane fuel (MON of 99.6) and modifications are 45 necessary in order to use lower-octane fuel. Automotive gasoline can vaporize in fuel lines causing a vapor lock (a bubble in the line) or fuel pump cavitation, starving the engine of fuel. Vapor lock typically occurs in fuel systems where a mechanically-driven fuel pump mounted on the engine draws 50 fuel from a tank mounted lower than the pump. The reduced pressure in the line can cause the more volatile components in automotive gasoline to flash into vapor, forming bubbles in the fuel line and interrupting fuel flow.

The ASTM D910 specification does not include all gasoline satisfactory for reciprocating aviation engines, but rather, defines the following specific types of aviation gasoline for civil use: Grade 80; Grade 91; Grade 100; and Grade 100LL. Grade 100 and Grade 100LL are considered High Octane Aviation Gasoline to meet the requirement of modern 60 demanding aviation engines. In addition to MON, the D910 specification for Avgas have the following requirements: density; distillation (initial and final boiling points, fuel evaporated, evaporated temperatures T₁₀, T₄₀, T₉₀, T₁₀+T₅₀); recovery, residue, and loss volume; vapor pressure; freezing 65 point; sulfur content; net heat of combustion; copper strip corrosion; oxidation stability (potential gum and lead precipi-

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tate); volume change during water reaction; and electrical conductivity. Avgas fuels are typically tested for its properties using ASTM tests:

Motor Octane Number: ASTM D2700

Aviation Lean Rating: ASTM D2700

Performance Number (Super-Charge): ASTM D909

Tetraethyl Lead Content: ASTM D5059 or ASTM D3341

Color: ASTM D2392

Density: ASTM D4052 or ASTM D1298

Distillation: ASTM D86

Vapor Pressure: ASTM D5191 or ASTM D323 or ASTM D5190

Freezing Point: ASTM D2386

Sulfur: ASTM D2622 or ASTM D1266

Net Heat of Combustion (NHC): ASTM D3338 or ASTM D4529 or ASTM D4809

Copper Corrosion: ASTM D130

Oxidation Stability—Potential Gum: ASTM D873

Oxidation Stability—Lead Precipitate: ASTM D873

Water Reaction—Volume change: ASTM D1094

Electrical Conductivity: ASTM D2624

Aviation fuels must have a low vapor pressure in order to avoid problems of vaporization (vapor lock) at low pressures encountered at altitude and for obvious safety reasons. But the vapor pressure must be high enough to ensure that the engine starts easily. The Reid Vapor pressure (RVP) should be in the range of 38 kPa to 49 kPA. The final distillation point must be fairly low in order to limit the formations of deposits and their harmful consequences (power losses, impaired cooling). These fuels must also possess a sufficient Net Heat of Combustion (NHC) to ensure adequate range of the aircraft. Moreover, as aviation fuels are used in engines providing good performance and frequently operating with a high load, i.e. under conditions close to knocking, this type of fuel is expected to have a very good resistance to spontaneous combustion.

Moreover, for aviation fuel two characteristics are determined which are comparable to octane numbers: one, the MON or motor octane number, relating to operating with a slightly lean mixture (cruising power), the other, the Octane rating, Performance Number or PN, relating to use with a distinctly richer mixture (take-off). With the objective of guaranteeing high octane requirements, at the aviation fuel production stage, an organic lead compound, and more particularly tetraethyllead (TEL), is generally added. Without the TEL added, the MON is typically around 91. As noted above ASTM D910, 100 octane aviation fuel requires a minimum motor octane number (MON) of 99.6. The distillation profile of the high octane unleaded aviation fuel composition should have a T10 of maximum 75° C., T40 of minimum 75° C., T50 of maximum 105° C., and T90 of maximum 135° C.

As in the case of fuels for land vehicles, administrations are tending to lower the lead content, or even to ban this additive, due to it being harmful to health and the environment. Thus, the elimination of lead from the aviation fuel composition is becoming an objective.

SUMMARY OF THE INVENTION

It has been found that it is difficult to produce a high octane unleaded aviation fuel that meet most of the ASTM D910 specification for high octane aviation fuel. In addition to the MON of 99.6, it is also important to not negatively impact the flight range of the aircraft, vapor pressure, temperature profile and freeze points that meet the aircraft engine start up requirements and continuous operation at high altitude.

In accordance with certain of its aspects, in one embodiment of the present invention provides an unleaded aviation fuel composition having a MON of at least 99.6, sulfur content of less than 0.05 wt %, CHN content of at least 97.8 wt %, less than 2.2 wt % of oxygen content, a T10 of at most 75° C., 5 T40 of at least 75° C., a T50 of at most 105° C., a T90 of at most 135° C., a final boiling point of less than 190° C., an adjusted heat of combustion of at least 43.5 MJ/kg, a vapor pressure in the range of 38 to 49 kPa, comprising a blend comprising:

from about 35 vol. % to about 55 vol. % of toluene having a MON of at least 107; from about 2 vol. % to about 10 vol. % of aniline;

from about 15 vol % to about 30 vol % of at least one alkylate or alkyate blend having an initial boiling range of from about 32° C. to about 60° C. and a final boiling range of from about 105° C. to about 140° C., having T40 of less than 99° C., T50 of less than 100° C., T90 of less than 110° C. the alkylate or alkylate blend comprising isoparaffins from 4 to 9 carbon atoms, about 3-20 vol 20 % of C5 isoparaffins, about 3-15 vol % of C7 isoparaffins, and about 60-90 vol % of C8 isoparaffins, based on the alkylate or alkylate blend, and less than 1 vol % of C10+, based on the alkylate or alkylate blend;

from about 4 vol % to about 10 vol % of an alcohol having 25 a boiling point in the range of 80° C. to 140° C. and having 4 to 5 carbon numbers; and

at least 8 vol % of isopentane in an amount sufficient to reach a vapor pressure in the range of 38 to 49 kPa; wherein the fuel composition contains less than 1 vol % of C8 30 aromatics.

The features and advantages of the invention will be apparent to those skilled in the art. While numerous changes may be made by those skilled in the art, such changes are within the spirit of the invention.

BRIEF DESCRIPTION OF THE DRAWINGS

This drawing illustrates certain aspects of some of the or define the invention.

FIG. 1 shows the engine conditions for unleaded aviation fuel Example 3 at 2575 RPM at constant manifold pressure.

FIG. 2 shows the detonation data for unleaded aviation fuel Example 3 at 2575 RPM at constant manifold pressure.

FIG. 3 shows the engine conditions for unleaded aviation fuel Example 3 at 2400 RPM at constant manifold pressure.

FIG. 4 shows the detonation data for unleaded aviation fuel Example 3 at 2400 RPM at constant manifold pressure.

FIG. 5 shows the engine conditions for unleaded aviation 50 fuel Example 3 at 2200 RPM at constant manifold pressure. FIG. 6 shows the detonation data for unleaded aviation fuel

Example 3 at 2200 RPM at constant manifold pressure.

FIG. 7 shows the engine conditions for unleaded aviation fuel Example 3 at 2757 RPM at constant power.

FIG. 8 shows the detonation data for unleaded aviation fuel Example 3 at 2757 RPM at constant power.

FIG. 9 shows the engine conditions for FBO sourced 100LL fuel at 2575 RPM at constant manifold pressure.

FIG. 10 shows the detonation data for FBO sourced 100LL 60 fuel at 2575 RPM at constant manifold pressure.

FIG. 11 shows the engine conditions for FBO sourced 100LL fuel at 2400 RPM at constant manifold pressure.

FIG. 12 shows the detonation data for FBO sourced 100LL fuel at 2400 RPM at constant manifold pressure.

FIG. 13 shows the engine conditions for FBO sourced 100LL fuel at 2200 RPM at constant manifold pressure.

FIG. 14 shows the detonation data for FBO sourced 100LL fuel at 2200 RPM at constant manifold pressure.

FIG. 15 shows the engine conditions for FBO sourced 100LL fuel at 2757 RPM at constant power.

FIG. 16 shows the detonation data for FBO sourced 100LL fuel at 2757 RPM at constant power.

DETAILED DESCRIPTION OF THE INVENTION

We have found that a high octane unleaded aviation fuel having an aromatics content measured according to ASTM D5134 of from about 40 wt % to about 55 wt % and oxygen content of less than 2.2 wt %, based on the unleaded aviation fuel blend that meets most of the ASTM D910 specification for 100 octane aviation fuel can be produced by a blend comprising from about 35 vol % to about 55 vol % of high MON toluene, from about 2 vol % to about 10 vol % of aniline, from about 15 vol % to about 30 vol %, of at least one alkylate cut or alkylate blend that have certain composition and properties, at least 8 vol % of isopentane and from about 4 vol % to about 10 vol % of an alcohol having a boiling point in the range of 80° C. to 140° C. and having 4 to 5 carbon numbers. In an embodiment no ethanol is present in the high octane unleaded aviation fuel composition. The high octane unleaded aviation fuel of the invention has a MON of greater than 99.6.

Further the unleaded aviation fuel composition contains less than 1 vol %, preferably less than 0.5 vol % of C8 aromatics. It has been found that C8 aromatics such as xylene may have materials compatibility issues, particularly in older aircraft. Further it has been found that unleaded aviation fuel containing C8 aromatics tend to have difficulties meeting the temperature profile of D910 specification. In another embodiment, the unleaded aviation fuel contains no alcohol boiling less than 80° C. In another embodiment, the unleaded aviation fuel contains no noncyclic ethers. Further, the unleaded aviation fuel composition has a benzene content between 0% v and 5% v, preferably less than 1% v.

In another embodiment, the unleaded aviation fuel conembodiments of the invention, and should not be used to limit 40 tains no alcohol boiling less than 80° C. Further, in some embodiments, the volume change of the unleaded aviation fuel tested for water reaction is within +/-2 mL as defined in ASTM D1094.

> The high octane unleaded fuel will not contain lead and preferably not contain any other metallic octane boosting lead equivalents. The term "unleaded" is understood to contain less than 0.01 g/L of lead. The high octane unleaded aviation fuel will have a sulfur content of less than 0.05 wt %. In some embodiments, it is preferred to have ash content of less than 0.0132 g/L (0.05 g/gallon) (ASTM D-482).

According to current ASTM D910 specification, the NHC should be close to or above 43.5 mJ/kg. The Net Heat of Combustion value is based on a current low density aviation fuel and does not accurately measure the flight range for 55 higher density aviation fuel. It has been found that for unleaded aviation gasolines that exhibit high densities, the heat of combustion may be adjusted for the higher density of the fuel to more accurately predict the flight range of an

There are currently three approved ASTM test methods for the determination of the heat of combustion within the ASTM D910 specification. Only the ASTM D4809 method results in an actual determination of this value through combusting the fuel. The other methods (ASTM D4529 and ASTM D3338) are calculations using values from other physical properties. These methods have all been deemed equivalent within the ASTM D910 specification.

Currently the Net Heat of Combustion for Aviation Fuels (or Specific Energy) is expressed gravimetrically as MJ/kg. Current lead containing aviation gasolines have a relatively low density compared to many alternative unleaded formulations. Fuels of higher density have a lower gravimetric energy 5 content but a higher volumetric energy content (MJ/L).

The higher volumetric energy content allows greater energy to be stored in a fixed volume. Space can be limited in general aviation aircraft and those that have limited fuel tank capacity, or prefer to fly with full tanks, can therefore achieve 10 greater flight range. However, the more dense the fuel, then the greater the increase in weight of fuel carried. This could result in a potential offset of the non-fuel payload of the aircraft. Whilst the relationship of these variables is complex, the formulations in this embodiment have been designed to 15 best meet the requirements of aviation gasoline. Since in part density effects aircraft range, it has been found that a more accurate aircraft range, normally gauged using Heat of Combustion, can be predicted by adjusting for the density of the avgas using the following equation:

HOC*=(HOC,/density)+(% range increase/% payload increase+1)

where HOC* is the adjusted Heat of Combustion (MJ/kg), HOC $_{\nu}$ is the volumetric energy density (MJ/L) obtained from 25 actual Heat of Combustion measurement, density is the fuel density (g/L), % range increase is the percentage increase in aircraft range compared to $100\,\mathrm{LL}$ (HOC $_{LL}$) calculated using HOC $_{\nu}$ and HOC $_{LL}$ for a fixed fuel volume, and % payload increase is the corresponding percentage increase in payload 30 capacity due to the mass of the fuel.

The adjusted heat of combustion will be at least 43.5 MJ/kg, and have a vapor pressure in the range of 38 to 49 kPa. The high octane unleaded fuel composition will further have a freezing point of -58° C. or less. Unlike for automobile 35 fuels, for aviation fuel, due to the altitude while the plane is in flight, it is important that the fuel does not cause freezing issues in the air. It has been found that for unleaded fuels containing aromatic amines such as Comparative Examples D and H in the Examples, it is difficult to meet the freezing point requirement of aviation fuel. It has been found that the aviation fuel composition containing an branched chain alcohol having 4 to 8 carbon atoms provided that the branched chain does not include t-butyl group provides unleaded aviation fuel that meets the freezing point requirement of -58° C. 45

Further, the final boiling point of the high octane unleaded fuel composition should be less than 190° C., preferably at most 180° C. measured with greater than 98.5% recovery as measured using ASTM D-86. If the recovery level is low, the final boiling point may not be effectively measured for the 50 composition (i.e., higher boiling residual still remaining rather than being measured). The high octane unleaded aviation fuel composition of the invention have a Carbon, Hydrogen, and Nitrogen content (CHN content) of at least 97.8 wt %, preferably at least 98.5 wt %, and less than 2.2 wt %, 55 preferably less than 1.5 wt % of oxygen-content.

It has been found that the high octane unleaded aviation fuel of the invention not only meets the MON value for 100 octane aviation fuel, but also meets the freeze point and the temperature profile of T10 of at most 75° C., T40 of at least 60 75° C., T50 at most 105° C., and T90 of at most 135° C., vapor pressure, adjusted heat of combustion, and freezing point. In addition to MON it is important to meet the minimum vapor pressure, and minimum adjusted heat of combustion for aircraft engine start up and smooth operation of the plane at 65 higher altitude. Preferably the potential gum value is less than 6 mg/100 mL.

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It is difficult to meet the demanding specification for unleaded high octane aviation fuel. For example, U.S. Patent Application Publication 2008/0244963, discloses a lead-free aviation fuel with a MON greater than 100, with major components of the fuel made from avgas and a minor component of at least two compounds from the group of esters of at least one mono- or poly-carboxylic acid and at least one mono- or polyol, anhydrides of at least one mono- or poly carboxylic acid. These oxygenates have a combined level of at least 15% v/v, typical examples of 30% v/v, to meet the MON value. However, these fuels do not meet many of the other specifications such as heat of combustion (measured or adjusted) at the same time, including even MON in many examples. Another example, U.S. Pat. No. 8,313,540 discloses a biogenic turbine fuel comprising mesitylene and at least one alkane with a MON greater than 100. However, these fuels also do not meet many of the other specifications such as heat of combustion (measured or adjusted), temperature profile, and vapor pressure at the same time.

Toluene

Toluene occurs naturally at low levels in crude oil and is usually produced in the processes of making gasoline via a catalytic reformer, in an ethylene cracker or making coke from coal. Final separation, either via distillation or solvent extraction, takes place in one of the many available processes for extraction of the BTX aromatics (benzene, toluene and xylene isomers). The toluene used in the invention must be a grade of toluene that have a MON of at least 107 and containing less than 1 vol % of C8 aromatics. Further, the toluene component preferably has a benzene content between 0% v and 5% v, preferably less than 1% v.

For example an aviation reformate is generally a hydrocarbon cut containing at least 70% by weight, ideally at least 85% by weight of toluene, and it also contains C8 aromatics (15 to 50% by weight ethylbenzene, xylenes) and C9 aromatics (5 to 25% by weight propyl benzene, methyl benzenes and trimethylbenzenes). Such reformate has a typical MON value in the range of 102-106, and it has been found not suitable for use in the present invention.

Toluene is preferably present in the blend in an amount from about 35% v, preferably at least about 40% v, most preferably at least about 42% v to at most about 48% v, preferably to at most about 55% v, more preferably to at most about 50% v, based on the unleaded aviation fuel composition.

Aniline

Aniline ($C_6H_5NH_2$) is mainly produced in industry in two steps from benzene. First, benzene is nitrated using a concentrated mixture of nitric acid and sulfuric acid at 50 to 60° C., which gives nitrobenzene. In the second step, the nitrobenzene is hydrogenated, typically at 200-300° C. in presence of various metal catalysts.

As an alternative, aniline is also prepared from phenol and ammonia, the phenol being derived from the cumene process.

In commerce, three brands of aniline are distinguished: aniline oil for blue, which is pure aniline; aniline oil for red, a mixture of equimolecular quantities of aniline and orthoand para-toluidines; and aniline oil for safranine, which contains aniline and ortho-toluidine, and is obtained from the distillate (échappés) of the fuchsine fusion. Pure aniline, otherwise known as aniline oil for blue is desired for high octane unleaded avgas. Aniline is preferably present in the blend in an amount from about 2% v, preferably at least about 3% v,

most preferably at least about 4% v to at most about 10% v, preferably to at most about 7%, more preferably to at most about 6%, based on the unleaded aviation fuel composition.

Alkylate and Alkyate Blend

The term alkylate typically refers to branched-chain paraffin. The branched-chain paraffin typically is derived from the reaction of isoparaffin with olefin. Various grades of branched chain isoparaffins and mixtures are available. The grade is 10 identified by the range of the number of carbon atoms per molecule, the average molecular weight of the molecules, and the boiling point range of the alkylate. It has been found that a certain cut of alkylate stream and its blend with isoparaffins such as isooctane is desirable to obtain or provide the high octane unleaded aviation fuel of the invention. These alkylate or alkylate blend can be obtained by distilling or taking a cut of standard alkylates available in the industry. It is optionally blended with isooctane. The alkylate or alkyate blend have an initial boiling range of from about 32° C. to about 60° C. and $\,^{20}$ a final boiling range of from about 105° C. to about 140° C., preferably to about 135° C., more preferably to about 130° C., most preferably to about 125° C.), having T40 of less than 99° C., preferably at most 98° C., T50 of less than 100° C., T90 of less than 110° C., preferably at most 108° C., the alkylate or 25 alkylate blend comprising isoparaffins from 4 to 9 carbon atoms, about 3-20 vol % of C5 isoparaffins, based on the alkylate or alkylate blend, about 3-15 vol % of C7 isoparaffins, based on the alkylate or alkylate blend, and about 60-90 vol % of C8 isoparaffins, based on the alkylate or alkylate 30 blend, and less than 1 vol % of C10+, preferably less than 0.1 vol %, based on the alkylate or alkylate blend. Alkylate or alkylate blend is preferably present in the blend in an amount from about 15% v, preferably at least about 17% v, most preferably at least about 22% v to at most about 49% $v,\ ^{35}$ preferably to at most about 30% v, more preferably to at most about 25% v.

Isopentane

Isopentane is present in an amount of at least 8 vol % in an amount sufficient to reach a vapor pressure in the range of 38 to 49 kPa. The alkylate or alkylate blend also contains C5 isoparaffins so this amount will typically vary between 5 vol % and 25 vol % depending on the C5 content of the alkylate or alkylate blend. Isopentane should be present in an amount to reach a vapor pressure in the range of 38 to 49 kPa to meet aviation standard. The total isopentane content in the blend is typically in the range of 10% to 26 vol %, preferably in the range of 17% to 23% by volume, based on the aviation fuel 50 composition.

Co-Solvent

The unleaded aviation fuel contains an alcohol having a boiling point in the range of 80° C. to 140° C. and having 4 to 5 carbon atoms, preferably having 4 carbon atoms. The boiling point of alcohol is at least 80° C., preferably at least 90° C., to at most 140° C., to preferably at most 130° C., more preferably at most 120° C. The alcohol may contain mixtures of alcohols as long as the alcohols meet the boiling point and carbon number requirements. The co-solvent is present in an amount from about from about 4 vol % to about 10 vol %, preferably from about 4 vol % to about 7 vol %. Suitable co-solvent may be, for example, iso-butanol, n-butanol, t-butanol, 1-pentanol, 2-pentanol, 3-pentanol, 2-methyl-1-butanol or mixtures thereof. The alcohol may prefer

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ably be a C4 alcohol or a mixture of C4 alcohols. The unleaded aviation fuels containing aromatic amines tend to be significantly more polar in nature than traditional aviation gasoline base fuels. As a result, they have poor solubility in the fuels at low temperatures, which can dramatically increase the freeze points of the fuels. Consider for example an aviation gasoline base fuel comprising 10% v/v isopentane, 70% v/v light alkylate and 20% v/v toluene. This blend has a MON of around 90 to 93 and a freeze point (ASTM D2386) of less than -76° C. The addition of 6% w/w (approximately 4% v/v) of the aromatic amine aniline increases the MON to 96.4. At the same time, however, the freeze point of the resultant blend (again measured by ASTM D2386) increases to -12.4° C. The current standard specification for aviation gasoline, as defined in ASTM D910, stipulates a maximum freeze point of -58° C. Therefore, simply replacing TEL with a relatively large amount of an alternative aromatic octane booster would not be a viable solution for an unleaded aviation gasoline fuel. It has been found that alcohols having a boiling point in the range of 80° C. to 140° C. and having 4 to 5 carbon atoms dramatically decrease the freezing point of the unleaded aviation fuel to meet the current ASTM D910 standard for aviation fuel.

Preferably the water reaction volume change is within +/-2 ml for aviation fuel. Water reaction volume change is large for ethanol that makes ethanol not suitable for aviation gasoline.

Blending

For the preparation of the high octane unleaded aviation gasoline, the blending can be in any order as long as they are mixed sufficiently. It is preferable to blend the polar components into the toluene, then the non-polar components to complete the blend. For example the aromatic amine and co-solvent are blended into toluene, followed by isopentane and alkylate component (alkylate or alkylate blend).

In order to satisfy other requirements, the unleaded aviation fuel according to the invention may contain one or more additives which a person skilled in the art may choose to add from standard additives used in aviation fuel. There should be mentioned, but in non-limiting manner, additives such as antioxidants, anti-icing agents, antistatic additives, corrosion inhibitors, dyes and their mixtures.

According to another embodiment of the present invention a method for operating an aircraft engine, and/or an aircraft which is driven by such an engine is provided, which method involves introducing into a combustion region of the engine the high octane unleaded aviation gasoline fuel formulation described herein. The aircraft engine is suitably a spark ignition piston-driven engine. A piston-driven aircraft engine may for example be of the inline, rotary, V-type, radial or horizontally-opposed type.

While the invention is susceptible to various modifications and alternative forms, specific embodiments thereof are shown by way of examples herein described in detail. It should be understood, that the detailed description thereto are not intended to limit the invention to the particular form disclosed, but on the contrary, the intention is to cover all modifications, equivalents and alternatives falling within the spirit and scope of the present invention as defined by the appended claims. The present invention will be illustrated by the following illustrative embodiment, which is provided for illustration only and is not to be construed as limiting the claimed invention in any way.

| US 9 | 9,127,22 | 5 B2 | |
|---|----------------------|--|----------------|
| 9 | | 10 | |
| ILLUSTRATIVE EMBODIMENT | | -continued | |
| | _ | Continued | |
| Test Methods | | T50 (deg C.) T90 (deg C.) | 103.9 114.6 |
| | | FBP (deg C.) | 179.5 |
| The following test methods were used for the measurement | tof ⁵ — | | |
| the aviation fuels. | | | |
| Motor Octane Number: ASTM D2700 Tetraethyl Lead Content: ASTM D5059 | | Example 2 | |
| Density: ASTM D4052 | | • | |
| Distillation: ASTM D86 | 10 | isopentane | 22% v |
| Vapor Pressure: ASTM D323 | | narrow cut alkylate | 11% v |
| Freezing Point: ASTM D2386 | | Isooctane toluene | 11% v 45% v |
| Sulfur: ASTM D2622 | | aniline | 6% v |
| Net Heat of Combustion (NHC): ASTM D3338 | 1.5 | t-butanol | 5% v |
| Copper Corrosion: ASTM D130 | 15 — | Property | |
| Oxidation Stability—Potential Gum: ASTM D873 Oxidation Stability—Lead Precipitate: ASTM D873 | _ | 1607 | 100.4 |
| Water Reaction—Volume change: ASTM D1094 | | MON RVP (kPa) | 102.4 48.9 |
| Detail Hydrocarbon Analysis (ASTM 5134) | | Freeze Point (deg C.) | <-70.5 |
| | 20 | Lead Content (g/gal) Density (g/mL) | <0.01 0.786 |
| Examples 1-4 | | Net Heat of | 41.96 |
| | | Combustion (MJ/kg) | 42.52 |
| The aviation fuel compositions of the invention we blended as follows. Toluene having 107 MON (from Y | | Adjusted Net Heat of Combustion (MJ/kg) | 43.53 |
| Racing Fuels Inc.) was mixed with Aniline (from Univar N | | T10 (deg C.) | 56.9 |
| while mixing. | | T40 (deg C.) T50 (deg C.) | 96.9 103.9 |
| Isooctane (from Univar NV) and Narrow Cut Alkyl | ate | T90 (deg C.) | 114.4 |
| having the properties shown in Table below (from Shell No | | FBP (deg C.) | 175.4 |
| erland Chemie BV) were poured into the mixture in no p | | | |
| ticular order. Then, butanol (from Univar NV) was add | | | |
| followed by isopentane (from Matheson Tri-Gas, Inc.) | to | Example 3 | |
| complete the blend. | | Example 3 | |
| TABLE 1 | | | |
| | — 35 — | | |
| Narrow Cut Alkylate Blend Properties | _ | isopentane narrow cut alkylate | 21% v 12% v |
| IBP (ASTM D86, ° C.) 39.1 | | Isooctane | 12% v |
| FBP (ASTM D86, ° C.) 115.1 T40 (ASTM D86, ° C.) 94.1 | | toluene aniline | 45% v 5% v |
| T50 (ASTM D86, ° C.) 98 | 40 | isobutanol | 5% v |
| T90 (ASTM D86, ° C.) 105.5 Vol % iso-C5 14.52 | | Dronouter | |
| Vol % iso-C3 14.32 Vol % iso-C7 7.14 | _ | Property | |
| Vol % iso-C8 69.35 | | MON | 103.7 |
| Vol % C10+ 0 | | RVP (kPa) Freeze Point (deg C.) | 44.1 <-65.5 |
| | 45 | Lead Content (g/gal) | <0.01 |
| Example 1 | | Density (g/mL) Net Heat of | 0.779 42.13 |
| Example 1 | | Combustion (MJ/kg) | |
| | | Adjusted Net Heat of Combustion (MJ/kg) | 43.70 |
| | 50 | Water Reaction | -1 |
| isopentane 22% v narrow cut alkylate 11% v | | T10 (deg C.) | 65.5 |
| Isooctane 11% v | | T40 (deg C.) T50 (deg C.) | 101.0 104 |
| toluene 45% v | | T90 (deg C.) | 115.5 |
| aniline 6% v 1-butanol 5% v | 55 — | FBP (deg C.) | 179.5 |
| | | | |
| Property | | Example 4 | |
| MON 100 | | Ехатріе 4 | |
| RVP (kPa) 49.0 Freeze Point (deg C.) <-70.5 | | | |
| Lead Content (g/gal) <0.01 | 60 | | |
| Density (g/mL) 0.787 Net Heat of 41.99 | | isopentane | 21% v 12% v |
| Net Heat of 41.99 Combustion (MJ/kg) | | narrow cut alkylate Isooctane | 12% V 11% v |
| Adjusted Net Heat of 43.57 | | toluene | 45% v |
| Combustion (MJ/kg) T10 (deg C.) 60.7 | 65 | aniline isobutanol | 6% v 5% v |
| T40 (deg C.) 00.7 T40 (deg C.) 100.8 | _ | is continued | 570 V |
| | | | |

-continued

| Property | |
|-----------------------|--------|
| MON | 101.9 |
| RVP (kPa) | 38.54 |
| Freeze Point (deg C.) | -70 |
| Lead Content (g/gal) | < 0.01 |
| Density (g/mL) | 0.81 |
| Net Heat of | 41.95 |
| Combustion (MJ/kg) | |
| Adjusted Net Heat of | 43.61 |
| Combustion (MJ/kg) | |
| T10 (deg C.) | 72.4 |
| T40 (deg C.) | 101.4 |
| T50 (deg C.) | 103.7 |
| T90 (deg C.) | 117.3 |
| FBP (deg C.) | 179.8 |

Properties of an Alkylate Blend

Properties of an alkyalte blend containing ½ narrow cut alkylate (having properties as shown above) and ½ Isooctane is shown in Table 2 below.

TABLE 2

| Alkylate Blend Properties | |
|---------------------------|-------|
| IBP (ASTM D86, ° C.) | 54.0 |
| FBP (ASTM D86, ° C.) | 117.5 |
| T40 (ASTM D86, ° C.) | 97.5 |
| T50 (ASTM D86, ° C.) | 99.0 |
| T90 (ASTM D86, ° C.) | 102.5 |
| Vol % iso-C5 | 5.17 |
| Vol % iso-C7 | 3.60 |
| Vol % iso-C8 | 86.83 |
| Vol % C10+ | 0.1 |

Combustion Properties

In addition to the physical characteristics, an aviation gasoline should perform well in a spark ignition reciprocating aviation engine. A comparison to the current leaded aviation gasoline found commercially is the simplest way to assess the combustion properties of a new aviation gasoline.

Table 3 below provides the measured operating parameters on a Lycoming TIO-540 J2BD engine for avgas Example 3 and a commercially purchased 100 LL avgas (FBO100LL).

3 was generated using a Lycoming TIO-540 J2BD six cylinder reciprocating aviation piston engine mounted on an engine test dynamometer. Of particular note are the fuel consumption values. Given the higher density of the fuel, it would be expected that the test fuel would require significantly higher fuel consumption in order to provide the same power to the engine. It is clear from Table 3 that the observed fuel consumption values are very similar across all test conditions, further supporting the use of an adjusted heat of combustion (HOC*) to compensate for fuel density effects in the evaluation of a fuel's impact on the range of an aircraft.

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In order to assure transparency with the existing leaded gasoline, the ability of an aviation engine to operate within its certified operating parameters when using an unleaded aviation fuel, such as cylinder head temperatures and turbine inlet temperatures over a range of air/fuel mixtures, was assessed using engine certification test normally submitted to FAA for a new engine. The test was run for unleaded aviation fuel Example 3 which results are shown in FIGS. 1 to 8 and for a commercial 100 LL fuel shown in FIGS. 9 to 16. The detonation data were obtained using the procedure specified in ASTM D6424. As can be seen in FIGS. 1, 3, 5 and 7 for the Example 3 test fuel and FIGS. 9, 11, 13 and 15 for the FBO sourced 100LL (101MON) reference fuel, the Lycoming IO 540 J2BD engine was able to operate over its entire certified operating range without issue using aviation fuel of Example 3 with no noticeable change in operating characteristics from operation with the 100LL reference fuel.

In order to fully evaluate the ability of an engine to operate correctly using a given fuel over its entire operating range, the resistance of the fuel to detonate must be included. Therefore, the fuel was evaluated for detonation against an FBO procured 100LL reference fuel (101 MON) at four conditions, 2575 RPM at constant manifold pressure (Example 3 FIG. 2, 100LL reference FIG. 10), 2400 RPM at constant manifold pressure (Example 3 FIG. 4, 100LL reference FIG. 12), 2200 RPM at constant manifold pressure (Example 3 FIG. 6, 100LL reference FIG. 14) and 2757 RPM at constant power (Example 3 FIG. 8, 100LL reference FIG. 16). These conditions provide the most detonation sensitive operating regions for this engine, and cover both lean and rich operation.

As can be seen from the detonation plots referenced-above, the unleaded aviation fuel of the invention performs comparably to the current 100LL leaded aviation fuel. Of particular importance is that the unleaded fuel experiences detonation at lower fuel flow than the comparable leaded fuel. Additionally,

TABLE 3

| Fuel | Altitude (ft) | RPM | Fuel Consumption (lbs/hr) | CHT ^a , Cyl 1 (° F.) | Turbine Inlet Temperature (° F.) | Brake Horsepower (Observed) | Brake Specific Fuel Consumption (lb./hphr) |
|------------|------------------|---------|---------------------------------|------------------------------------|--|-----------------------------------|---|
| FBO 100 LL | 3000 | 2575.09 | 212.35 | 472 | 1533 | 330.45 | 0.642 |
| Example 3 | 3000 | 2574.96 | 267.97 | 451 | 1476 | 334.64 | 0.801 |
| FBO 100 LL | 6000 | 2199.98 | 128.42 | 457 | 1615 | 256.54 | 0.495 |
| Example 3 | 6000 | 2199.87 | 135.15 | 464 | 1642 | 259.04 | 0.521 |
| FBO 100 LL | 8000 | 2575.16 | 221.27 | 464 | 1544 | 350.76 | 0.632 |
| Example 3 | 8000 | 2575.02 | 218.72 | 455 | 1617 | 363.31 | 0.602 |
| FBO 100 LL | 12000 | 2400.01 | 184.19 | 461 | 1520 | 297.77 | 0.618 |
| Example 3 | 12000 | 2400.06 | 189.34 | 458 | 1564 | 302.52 | 0.628 |

*CHT = cylinder head temperature. Although testing was conducted on a six cylinder engine, the variation between 100 LL and Example 3 results were similar over all six cylinders, so only cylinder 1 values are used for representation. Reference FIGS. 1, 3, 5, 7, 9, 11, 13, and 15 for more complete data.

here provides similar engine operating characteristics compared to the leaded reference fuel. The data provided in Table

As can be seen from Table 3 that the invention described 65 when detonation does occur, this observed intensity of this effect is typically smaller than that found for the leaded reference firel.

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Comparative Examples A-L

Comparative Examples A and B

The properties of a high octane unleaded aviation gasoline that use large amounts of oxygenated materials as described in U.S. Patent Application Publication 2008/0244963 as Blend X4 and Blend X7 is provided. The reformate contained 14 vol % benzene, 39 vol % toluene and 47 vol % xylene.

| Comparative Example A Blend X4 | Vol % | Comparative Example B Blend X7 | Vol % | |
|--------------------------------------|-------|--------------------------------------|-------|---|
| Isopentane | 12.25 | Isopentane | 12.25 | _ |
| Aviation alkylate | 43.5 | Aviation alkylate | 43.5 | |
| Reformate | 14 | Reformate | 14 | |
| Diethyl carbonate | 15 | Diethyl carbonate | 8 | |
| m-toluidine | 3 | m-toluidine | 2 | |
| MIBK | 12.46 | MIBK | 10 | |
| | | phenatole | 10 | |

| Property | Blend X4 | Blend X7 | 2 |
|-----------------------|----------|----------|---|
| MON | 100.4 | 99.3 | |
| RVP (kPa) | 35.6 | 40.3 | |
| Freeze Point (deg C.) | -51.0 | -70.0 | |
| Lead Content (g/gal) | < 0.01 | < 0.01 | |
| Density (g/mL) | 0.778 | 0.781 | 3 |
| Net Heat of | 38.017 | 39.164 | |
| Combustion (MJ/kg) | | | |
| Adjusted Net Heat of | 38.47 | 39.98 | |
| Combustion (MJ/kg) | | | |
| Oxygen Content (% m) | 8.09 | 6.16 | |
| T10 (deg C.) | 73.5 | 73 | 3 |
| T40 (deg C.) | 102.5 | 104 | |
| T50 (deg C.) | 106 | 108 | |
| T90 (deg C.) | 125.5 | 152.5 | |
| FBP (deg C.) | 198 | 183 | |

The difficulty in meeting many of the ASTM D-910 specifications is clear given these results. Such an approach to developing a high octane unleaded aviation gasoline generally results in unacceptable drops in the heat of combustion value (>10% below ASTM D910 specification) and final boil- 45 ing point. Even after adjusting for the higher density of these fuels, the adjusted heat of combustion remains too low.

Comparative Examples C and D

A high octane unleaded aviation gasoline that use large amounts of mesitylene as described as Swift 702 in U.S. Pat. No. 8,313,540 is provided as Comparative Example C. A high octane unleaded gasoline as described in Example 4 of U.S. 55 Patent Application Publication Nos. US20080134571 and US20120080000 are provided as Comparative Example D.

| Comparative Example C | Vol % | Comparative Example D | Vol % | |
|--------------------------|-------|--------------------------|-------|--|
| Isopentane | 17 | Isopentane | 3.5 | |
| Mesitylene | 83 | Isooctane | 45.5 | |
| | | Toluene | 23 | |
| | | m-xylene | 21 | |
| | | aniline | 7 | |

| Property | Comparative Example C | Comparative Example D |
|-----------------------|--------------------------|--------------------------|
| MON | 105 | 104 |
| RVP (kPa) | 35.16 | 17.79 |
| Freeze Point (deg C.) | -20.5 | -41.5 |
| Lead Content (g/gal) | < 0.01 | < 0.01 |
| Density (g/mL) | 0.830 | 0.794 |
| Net Heat of | 41.27 | 42.20 |
| Combustion (MJ/kg) | | |
| Adjusted Net Heat of | 42.87 | 43.86 |
| Combustion (MJ/kg) | | |
| T10 (deg C.) | 74.2 | 100.4 |
| T40 (deg C.) | 161.3 | 108.3 |
| T50 (deg C.) | 161.3 | 110.4 |
| T90 (deg C.) | 161.3 | 141.6 |
| FBP (deg C.) | 166.8 | 180.2 |

As can be seen from the properties, the Freeze Point is too high for both Comparative Examples C&D.

Comparative Examples E-L

Other comparative examples where the components were varied are provided below. As can been seem from the above and below examples, the variation in composition resulted in at least one of MON being too low, RVP being too high or low, Freeze Point being too high, or Heat of Combustion being too

| Comparative Example E | Vol % | Comparative F | Vol % |
|--------------------------|-------|---------------|-------|
| Isopentane | 10 | Isopentane | 15 |
| Aviation alkylate | 60 | isooctane | 60 |
| m-xylene | 30 | toluene | 25 |

| Property | Comparative Example E | Comparative F |
|--|--------------------------|---------------|
| MON | 93.6 | 95.4 |
| RVP (kPa) | 40 | 36.2 |
| Freeze Point (deg C.) | <-80 | <-80 |
| Lead Content (g/gal) | < 0.01 | < 0.01 |
| Density (g/mL) | 0.738 | 0.730 |
| Net Heat of Combustion (MJ/kg) | 43.11 | 43.27 |
| Adjusted Net Heat of Combustion (MJ/kg) | 44.70 | 44.83 |
| T10 (deg C.) | 68.4 | 76.4 |
| T40 (deg C.) | 106.8 | 98.7 |
| T50 (deg C.) | 112 | 99.7 |
| T90 (deg C.) | 134.5 | 101.3 |
| FBP (deg C.) | 137.1 | 115.7 |

| _ | Comparative Example G | Vol % | Comparative Example H | Vol % |
|---|--------------------------|----------|---------------------------------|----------|
| | Isopentane Isooctane | 15 75 | Isopentane Aviation alkylate | 10 69 |
| ; | Toluene | 10 | toluene m-toluidine | 15 6 |

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| 15 | | | | 16 Comparative Example K | | |
|---|--------------------------|---|----|--|--|--|
| Property | Comparative Example G | Comparative Example H | _ | Comparative Exam | прие К | |
| MON | 96 | 100.8 | _ | isopentane | 15% v | |
| RVP (kPa) | 36.9 | 44.8 | 5 | isooctane | 17% v | |
| Freeze Point (deg C.) Lead Content (g/gal) | <-80 <0.01 | -28.5 <0.01 | | Narrow cut alkylate | 17% v | |
| Density (g/mL) | 0.703 | 0.729 | | toluene | 40% v | |
| Net Heat of | 44.01 | 43.53 | | aniline | 6% v | |
| Combustion (MJ/kg) | | 13.33 | | tetrahydrofuran | 5% v | |
| Adjusted Net Heat of | 45.49 | 45.33 | 10 | D | | |
| Combustion (MJ/kg) | | | | Property | | |
| Γ10 (deg C.) | 75.3 | 65 | | MON | 99.4 | |
| Γ40 (deg C.) | 97.1 | 96.3 | | RVP (kPa) | 40.2 | |
| Γ50 (deg C.) | 98.4 | 100.6 | | Freeze Point (deg C.) | <-70 | |
| Г90 (deg C.) | 99.1 | 112.9 | | Lead Content (g/gal) | < 0.01 | |
| FBP (deg C.) | 111.3 | 197.4 | 15 | Density (g/mL) | 0.79 | |
| | | | | Net Heat of | 42.11 | |
| | | | | Combustion (MJ/kg) | | |
| | | | | Adjusted Net Heat of | 43.73 | |
| Compara | tive Example I | | | Combustion (MJ/kg) | | |
| | | | | T10 (deg C.) | 66.5 | |
| | | | 20 | T40 (deg C.) | 99 | |
| | | | | T50 (deg C.) | 102.5 | |
| isopentane | | 16% v | | T90 (deg C.) FBP (deg C.) | 116.5 179.5 | |
| isooctane | | 15% v | | rar (ucg C.) | 179.3 | |
| Narrow cut alkylate | | 13% v | | | | |
| toluene | | 45% v | 25 | | | |
| aniline | | 6% v | 23 | 25 Comparative Example L | | |
| Isobutyl acetate | | 5% v | | | | |
| Property | | | _ | | | |
| MON | | 101.4 | _ | isopentane | 21% v | |
| RVP (kPa) | | 38.47 | 30 | narrow cut alkylate | 13% v | |
| Freeze Point (deg C. |) | -35 | | Isooctane | 12% v | |
| Lead Content (g/gal | | < 0.01 | | toluene | 45% v | |
| Density (g/mL) | , | 0.801 | | aniline | 6% v | |
| Net Heat of | | 41.839 | | 2-ethyl hexanol | 3% v | |
| Combustion (MJ/kg | | | | • | | |
| Adjusted Net Heat of Combustion (MJ/kg | | 43.45 | 35 | Property | | |
| T10 (deg C.) | | 71 | | MON | 101.1 | |
| T40 (deg C.) | | 104.5 | | RVP (kPa) | 37.37 | |
| T50 (deg C.) | | 106.5 | | Freeze Point (deg C.) Lead Content (g/gal) | -36.5 <0.01 | |
| T90 (deg C.) | | 118.5 190.5 | 40 | Density (g/mL) | 0.79 | |
| FBP (deg C.) | | 190.5 | 40 | Net Heat of | 41.96 | |
| | | | | Combustion (MJ/kg) | 71.70 | |
| | | | | Adjusted Net Heat of | 43.55 | |
| | | | | Combustion (MJ/kg) | | |
| Compara | tive Example J | ſ | | T10 (deg C.) | 72.5 | |
| | | | 45 | T40 (deg C.) | 104 | |
| | | | 10 | T50 (deg C.) | 105.6 | |
| | | | _ | T90 (deg C.) | 127.1 | |
| isopentane | | 16% v | | FBP (deg C.) | 177.3 | |
| isooctane | | 15% v | | | | |
| | | 13% v | | | | |
| Narrow cut alkylate | | 45% v | 50 | We claim: | | |
| toluene | | | | 1. An unleaded aviation fuel comp | osition having a MON | |
| toluene aniline | | 6% v | | | | |
| toluene | | | | at least 99.6, sulfur content of less | s than 0.05 wt %, Cl | |
| toluene aniline | | 6% v | | | s than 0.05 wt %, Cl han 2.2 wt % of oxys | |
| toluene aniline Tetra-butyl acetate Property MON | | 6% v 5% v | | at least 99.6, sulfur content of less content of at least 97.8 wt %, less t | s than 0.05 wt %, CI han 2.2 wt % of oxys dof at least 75° C., a T | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) |) | 6% v 5% v | | at least 99.6, sulfur content of less content of at least 97.8 wt %, less t content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most | s than 0.05 wt %, CI han 2.2 wt % of oxyg of at least 75° C., a T t 135° C., a final boil: | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. | | 6% v 5% v 101.6 38.96 -35 | | at least 99.6, sulfur content of less content of at least 97.8 wt %, less t content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boil ed heat of combustion | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal | | 6% v 5% v 101.6 38.96 -35 <0.01 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less t content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressure | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boiled heat of combustions in the range of 38 to | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal Density (g/mL) | | 6% v 5% v 101.6 38.96 -35 <0.01 0.795 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less t content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressurkPa, a freezing point of less than -5 | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boiled heat of combustions in the range of 38 to | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal Density (g/mL) Net Heat of |) | 6% v 5% v 101.6 38.96 -35 <0.01 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less t content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressur kPa, a freezing point of less than -5 comprising: | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boiled heat of combustion in the range of 38 to 8° C. comprising a ble | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal Density (g/mL) Net Heat of Combustion (MJ/kg |) | 6% v 5% v 101.6 38.96 -35 <0.01 0.795 41.938 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less to content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressurkPa, a freezing point of less than -5 comprising: (a) from about 35 vol.% to about 15° content of less than 25° content of less than 35° content | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boiled heat of combustion in the range of 38 to 8° C. comprising a ble | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal Density (g/mL) Net Heat of Combustion (MJ/kg Adjusted Net Heat of |)) if | 6% v 5% v 101.6 38.96 -35 <0.01 0.795 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less t content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressur kPa, a freezing point of less than -5 comprising: | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boiled heat of combustione in the range of 38 to 8° C. comprising a block of the street of the st | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal Density (g/mL) Net Heat of Combustion (MJ/kg |)) if | 6% v 5% v 101.6 38.96 -35 <0.01 0.795 41.938 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less to content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressurkPa, a freezing point of less than -5 comprising: (a) from about 35 vol.% to about 35 vol.% to about 36 vol.% to about 36 vol.% to about 37 vol.% to about 38 vol.% | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boiled heat of combustions in the range of 38 to 8° C. comprising a ble out 55 vol.% of tolue | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal Density (g/mL) Net Heat of Combustion (MJ/kg Adjusted Net Heat of Combustion (MJ/kg |)) if | 6% v 5% v 101.6 38.96 -35 <0.01 0.795 41.938 43.54 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less to content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressurkPa, a freezing point of less than -5 comprising: (a) from about 35 vol.% to about 107; (b) from about 2 vol.% to about 1 | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boilised heat of combustions in the range of 38 to 8° C. comprising a ble out 55 vol.% of tolue 0 vol.% of aniline; | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal Density (g/mL) Net Heat of Combustion (MJ/kg Adjusted Net Heat c Combustion (MJ/kg T10 (deg C.) |)) if | 6% v 5% v 101.6 38.96 -35 <0.01 0.795 41.938 43.54 72 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less to content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressurkPa, a freezing point of less than -5 comprising: (a) from about 35 vol.% to about 10 from about 2 vol.% to about 10 from about 15 vol.% to about 10 from abo | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boiled heat of combustions in the range of 38 to 8° C. comprising a ble out 55 vol.% of tolue 0 vol.% of aniline; 30 vol.% of at least of | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal Density (g/mL) Net Heat of Combustion (MJ/kg Adjusted Net Heat of Combustion (MJ/kg T10 (deg C.) T40 (deg C.) T50 (deg C.) T90 (deg C.) |)) if | 6% v 5% v 101.6 38.96 -35 <0.01 0.795 41.938 43.54 72 103.5 105.5 117.5 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less to content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressurkPa, a freezing point of less than -5 comprising: (a) from about 35 vol.% to about 10 from about 2 vol.% to about 10 from about 15 vol.% to about alkylate or alkyate blend having | s than 0.05 wt %, CI han 2.2 wt % of oxys 0 of at least 75° C., a T t 135° C., a final boiling the deat of combustions in the range of 38 to 8° C. comprising a ble out 55 vol.% of tolue 0 vol.% of aniline; 30 vol.% of at least of an initial boiling rar | |
| toluene aniline Tetra-butyl acetate Property MON RVP (kPa) Freeze Point (deg C. Lead Content (g/gal Density (g/mL) Net Heat of Combustion (MJ/kg Adjusted Net Heat of Combustion (MJ/kg T10 (deg C.) T40 (deg C.) T50 (deg C.) |)) if | 6% v 5% v 101.6 38.96 -35 <0.01 0.795 41.938 43.54 72 103.5 105.5 | 55 | at least 99.6, sulfur content of less content of at least 97.8 wt %, less to content, a T10 of at most 75° C., T40 of at most 105° C., a T90 of at most point of less than 190° C., an adjust at least 43.5 MJ/kg, a vapor pressurkPa, a freezing point of less than -5 comprising: (a) from about 35 vol.% to about 10 from about 2 vol.% to about 10 from about 15 vol.% to about 10 from abo | s than 0.05 wt %, CI han 2.2 wt % of oxyg 0 of at least 75° C., a T t 135° C., a final boiling the deat of combustions in the range of 38 to 8° C. comprising a ble out 55 vol.% of tolue 0 vol.% of aniline; 30 vol.% of at least of an initial boiling range. | |

- less than 110° C. the alkylate or alkylate blend comprising isoparaffins from 4 to 9 carbon atoms, about 3-20 vol.% of C5 isoparaffins, about 3-15 vol.% of C7 isoparaffins, and about 60-90 vol.% of C8 isoparaffins, based on the alkylate or alkylate blend, and less than 1 vol % of C10+, based on the alkylate or alkylate blend;
- (d) from about 4 vol.% to about 10 vol.% of an alcohol having a boiling point in the range of 80° C. to 140° C. and having 4 to 5 carbon numbers; and
- (e) at least 8 vol.% of isopentane in an amount sufficient to reach a vapor pressure in the range of 38 to 49 kPa;
- wherein the fuel composition contains less than 1 vol.% of C8 aromatics.
- 2. The unleaded aviation fuel composition of claim 1 wherein the total isopentane content in the blend of 10% to 26 vol %.
- 3. The unleaded aviation fuel composition of claim 1 having a potential gum of less than 6~mg/100~mL.
- 4. The unleaded aviation fuel composition of claim 1 $_{20}$ wherein less than 0.2 vol % of ethers are present.
- 5. The unleaded aviation fuel composition of claim 2 further comprising an aviation fuel additive.
- **6**. The unleaded aviation fuel composition of claim **1** wherein no alcohol having a boiling point of less than 80° C. ²⁵ is present.
- 7. The unleaded aviation fuel composition of claim 1 wherein the final boiling point is at most 180° C.

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- **8**. The unleaded aviation fuel composition of claim **1** wherein the alkylate or alkylate blend have a C10+ content of less than 0.1 vol % based on the alkylate or alkylate blend.
- 9. The unleaded aviation fuel composition of claim 1 wherein the alcohol is selected from the group consisting of iso-butanol, n-butanol, t-butanol, 1-pentanol, 2-pentanol, 3-pentanol, 2-methyl-1-butanol and mixtures thereof.
- 10. The unleaded aviation fuel composition of claim 1 wherein the alcohol have a boiling point in the range of 80° C. to 120° C.
- 11. The unleaded aviation fuel composition of claim 10 wherein the alcohol have a boiling point in the range of 90° C. to 120° C.
- 12. The unleaded aviation fuel composition of claim 10 wherein the alcohol is a C4 alcohol or a mixture thereof.
- 13. The unleaded aviation fuel composition of claim 10 wherein the alcohol is isobutanol.
- **14**. The unleaded aviation fuel composition of claim 1 having water reaction within +/-2 mL as defined in ASTM D1094.
- **15**. The unleaded aviation fuel composition of claim **9** wherein the alcohol is selected from the group consisting of iso-butanol, n-butanol, t-butanol, 2-pentanol, 3-pentanol, 2-methyl-1-butanol and mixtures thereof.
- **16**. The unleaded aviation fuel composition of claim **10** wherein the alcohol is selected from the group consisting of iso-butanol, n-butanol, t-butanol, 2-pentanol, 3-pentanol, and mixtures thereof.

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